

$$Fr = \frac{U^2}{Lg}$$

It represents the ratio of the inertia force to the gravitational forces.

Euler's Number (Pressure coefficient):—

$$\frac{1}{C_p} = \frac{1}{Eu} = \frac{\text{Inertial force}}{\text{Pressure force}} = \frac{\text{Mass} \times \text{Acceleration}}{\text{Pressure} \times \text{cross-sectional area}}$$

We know

$$\frac{\rho_2 (d^2q_2/dt^2)}{\rho_1 (d^2q_1/dt^2)} = \frac{\nabla_2 P_2}{\nabla_1 P_1}$$

$$\Rightarrow \frac{\nabla_2 P_2}{\rho_2 (d^2q_2/dt^2)} = \frac{\nabla_1 P_1}{\rho_1 (d^2q_1/dt^2)}$$

$$\Rightarrow \frac{P_2 / L_2}{\rho_2 U_2 / L_2 / U_2^2} = \frac{P_1 / L_1}{\rho_1 U_1 / L_1 / U_1^2}$$

$$\Rightarrow \frac{P_2}{\rho_2 U_2^2} = \frac{P_1}{\rho_1 U_1^2} = Eu$$

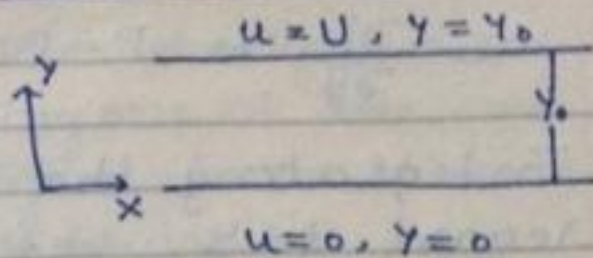
Thus in flows where inertia and pressure forces predominate, the pressure coefficient must be the same for dynamic similarity to exist.

Mach Number \Rightarrow The Perfect gas law and the velocity of sound is given by

$$P = \rho R T \Rightarrow \frac{\gamma P}{\rho} = \gamma R T = a^2$$

where a is the speed of sound

11.0 Laminar flow between Parallel Plates
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Consider two-dimensional laminar flow of an incompressible fluid of constant viscosity between two parallel plates at a distance y_0 . The system does not regard to z -axis.

The Equation of Continuity

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad \text{--- (1)}$$

$$\rho \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = - \frac{\partial p}{\partial x} + \rho g_x + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) \quad \text{--- (2)}$$

$$\rho \left(\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = - \frac{\partial p}{\partial y} + \rho g_y + \mu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) \quad \text{--- (3)}$$

The flow between these plates is taken to be in the x -direction.

then $v=0, w=0$ from the continuity equation, we have

$$\frac{\partial u}{\partial x} = 0 \Rightarrow u = u(y, t)$$

Hence the velocity depends on y and t . The steady state u depends on y only.

$$u = u(y), \quad v = 0 = w \quad \text{--- (4)}$$

From (2) and (3) we have

$$0 = - \frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial y^2} \quad \text{--- (5)}$$

$$0 = - \frac{\partial p}{\partial y}$$

From (6) we have

$$0 = -\frac{\partial P}{\partial y} \Rightarrow P = P(x)$$

Integrating the Equation (5) ^{two times} with regard to y , we have

$$\frac{d^2 u}{dy^2} = \frac{1}{\mu} \frac{dP}{dx}$$

$$\Rightarrow \frac{du}{dy} = \frac{1}{\mu} \frac{dP}{dx} y + A$$

$$\Rightarrow u = \frac{1}{2\mu} \frac{dP}{dx} y^2 + Ay + B \quad \text{--- (7)}$$

Where A and B are integration constant

Case I: Plane Couette flow:- the plane Couette flow or simple shear flow between two parallel plates. The upper plate is moving in x -direction with a uniform velocity U . At the lower plate

$$y=0, u=0 \Rightarrow B=0$$

At the upper plate $y=y_0, u=U$

We know $\mu \frac{d^2 u}{dy^2} = 0 \Rightarrow u(y) = Ay + B$

$$U = \frac{1}{2\mu} \frac{dP}{dx} \cdot 0 + Ay_0 + 0$$

$$Ay_0 = U$$

$$A = \frac{U}{y_0}$$

$$\text{i.e. } \frac{dP}{dx} = 0$$

We have

$$u = \frac{Uy}{y_0}$$

It follows that the velocity profile induced in a fluid by moving one of the boundaries at constant velocity is linear across the gap between two boundaries.

Case II :- Generalized Plane Couette flow :-

In this case either of two surface is moving at constant velocity and there is also an external Pressure gradient

$$\frac{dp}{dx} \neq 0$$

$$u = \frac{1}{2\mu} \frac{dp}{dx} y^2 + Ay + B$$

$$y = y_0$$

$$u = \frac{1}{2\mu} \frac{dp}{dx} y_0^2 + Ay_0 + B$$

$$u = \frac{1}{2\mu} \frac{dp}{dx} y_0^2 + Ay_0 \quad [B=0]$$

$$A = - \left\{ \frac{u}{y_0} + \frac{1}{2\mu} \frac{dp}{dx} y_0 \right\}$$

$$u(y) = \frac{uy}{y_0} - \frac{y_0^2}{2\mu} \frac{dp}{dx} \frac{y}{y_0} \left(1 - \frac{y}{y_0} \right)$$

$$\Rightarrow \frac{u(y)}{u} = \frac{y}{y_0} + \left(-\frac{y_0^2}{2\mu u} \frac{dp}{dx} \right) \frac{y}{y_0} \left(1 - \frac{y}{y_0} \right)$$

$$\frac{u(y)}{u} = \frac{y}{y_0} + P \frac{y}{y_0} \left(1 - \frac{y}{y_0} \right)$$

where $P = -\frac{y_0^2}{2\mu u} \frac{dp}{dx}$

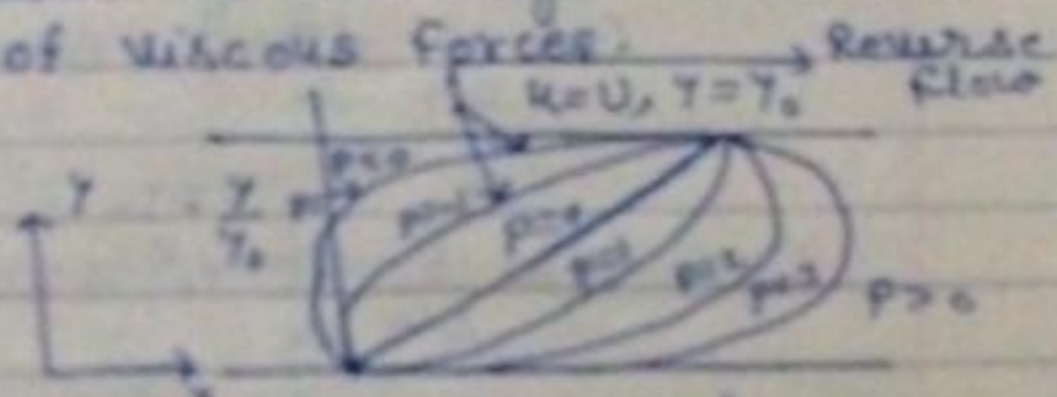
P is a dimensionless Pressure Parameter.

(i) $P > 0$ then $\frac{dp}{dx} < 0$ in the direction of flow

the velocity is +ve between the plates the pressure gradient will assist the viscosity induced motion to overcome the shear force at the lower plate.

(ii) $P < 0$ then $\frac{dp}{dx} > 0$ the pressure gradient is increasing in the direction of flow.

(iii) $P = 0$ the fluid motion in the +ve x-direction is entirely due to the action of viscous forces.



the average velocity distribution V

$$V = \frac{1}{\gamma_0} \int_0^{\gamma_0} u dy = U \int_0^{\gamma_0} \left\{ \frac{y}{\gamma_0} + P \frac{y}{\gamma_0} \left(1 - \frac{y}{\gamma_0} \right) \right\} dy$$

let $z = \frac{y}{\gamma_0}$ then $dz = \frac{1}{\gamma_0} dy$

$$V = U \int_0^1 [z + P(z - z^2)] dz$$

$$= \frac{U}{\gamma_0} \int_0^1 [z + Pz(1 - z)\gamma_0] dz$$

$$= U \left[\frac{1}{2} + P \left(\frac{1}{3} - \frac{1}{4} \right) \right]$$

$$= U \left[\frac{1}{2} + \frac{P}{6} \right]$$